

2nd method to determine the similarity parameters

differential equation of a problem \rightarrow example:

$$\frac{\partial p}{\partial x} = \gamma \frac{\partial^2 u}{\partial y^2}$$

① introduction of dimensionless values using reference values

example: $u_{ref} = u_{\infty}$; $\eta_{ref} = \eta_{\text{ref}}$; $h_{ref} = h$

$p_{ref} = \Delta p$; $L_{ref} = L$

$$\Rightarrow \bar{u} = \frac{u}{u_{ref}}; \bar{p} = \frac{p}{\Delta p}; \bar{\eta} = \frac{\eta}{\eta_{ref}}; \bar{x} = \frac{x}{L}; \bar{y} = \frac{y}{h}; \dots$$

$$\Rightarrow \boxed{\frac{\partial \bar{p}}{\partial \bar{x}} \frac{\partial \bar{p}}{\partial \bar{x}} = \frac{\eta_{ref} \cdot u_{ref}}{h^2} \cdot \bar{\eta} \frac{\partial^2 \bar{u}}{\partial \bar{y}^2}}$$

② divide the equation by the coefficient of one term \rightarrow dimensionless parameter

$$\boxed{\frac{\partial \bar{p}}{\partial \bar{x}} = \frac{L}{\Delta p} \frac{\eta_{ref} \cdot u_{ref}}{h^2} \cdot \bar{\eta} \frac{\partial^2 \bar{u}}{\partial \bar{y}^2}}$$

2 terms \rightarrow 1 parameter

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! method of dimensional analysis works as well \rightarrow gives maximum number of parameters

\rightarrow method of differential equation may provide less parameters

\rightarrow usually the parameters found can be expressed by known/ common parameters like Re, Eu, \dots

$$\frac{L \cdot \eta_{ref} \cdot u_{ref}}{\Delta p \cdot h^2} = \frac{\eta_{ref}}{g_{\text{Mach}}} \cdot \frac{g_{\text{Mach}}}{\Delta p} \cdot \frac{f}{h}$$

$\uparrow \quad \uparrow \quad \uparrow$
 $Re \quad Eu \quad \text{geometry}$

example: The governing equations for a laminar boundary layer flow of a flat plate are:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

(continuity)

$$g(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y}) = \gamma \frac{\partial^2 u}{\partial y^2}$$

(momentum)

$$g c_p (u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y}) = \lambda \frac{\partial^2 T}{\partial y^2}$$

(energy)

Hint: use the inflow conditions as reference

Determine the characterizing parameters of the problem and write them as functions of commonly known parameters.

$$\bar{u} = \frac{u}{u_{\infty}}; \bar{v} = \frac{v}{u_{\infty}}; \bar{g} = \frac{g}{g_{\infty}}; \bar{x} = \frac{x}{L}; \bar{y} = \frac{y}{L}; \bar{T} = \frac{T}{T_{\infty}}$$

$$\bar{\lambda} = \frac{\lambda}{\lambda_{\infty}}$$

$$\rightarrow \frac{u_{\infty}}{L} \left(\frac{\partial \bar{u}}{\partial \bar{x}} + \frac{\partial \bar{v}}{\partial \bar{y}} \right) = 0 \Rightarrow \text{no parameter}$$

$$\rightarrow g_{\infty} \frac{u_{\infty}^2}{L} \bar{g} \left(\bar{u} \frac{\partial \bar{u}}{\partial \bar{x}} + \bar{v} \frac{\partial \bar{u}}{\partial \bar{y}} \right) = \gamma_{\infty} \bar{g} \frac{u_{\infty}}{L^2} \frac{\partial^2 \bar{u}}{\partial \bar{y}^2}$$

$$\rightarrow \bar{g} \left(\bar{u} \frac{\partial \bar{u}}{\partial \bar{x}} + \bar{v} \frac{\partial \bar{u}}{\partial \bar{y}} \right) = \bar{g} \frac{\partial^2 \bar{u}}{\partial \bar{y}^2} \cdot \underbrace{\left(\frac{\gamma_{\infty} u_{\infty} L}{L^2 g_{\infty} u_{\infty}^2} \right)}_{K_1}$$

$$\rightarrow \frac{g_{\infty} c_{p_{\infty}} u_{\infty} T_{\infty}}{L} \bar{g} \bar{c}_p \left(\bar{u} \frac{\partial \bar{T}}{\partial \bar{x}} + \bar{v} \frac{\partial \bar{T}}{\partial \bar{y}} \right) = \frac{\lambda_{\infty} T_{\infty}}{L^2} \bar{g} \frac{\partial^2 \bar{T}}{\partial \bar{y}^2}$$

$$\rightarrow \bar{g} \bar{c}_p \left(\bar{u} \frac{\partial \bar{T}}{\partial \bar{x}} + \bar{v} \frac{\partial \bar{T}}{\partial \bar{y}} \right) = \bar{g} \frac{\partial^2 \bar{T}}{\partial \bar{y}^2} \cdot \underbrace{\left(\frac{\lambda_{\infty} T_{\infty} L}{L^2 g_{\infty} c_{p_{\infty}} u_{\infty} T_{\infty}} \right)}_{K_2}$$

$$K_2 = \underbrace{\frac{\lambda_{\infty}}{c_{p_{\infty}} \gamma_{\infty}}}_{1/\Pr} \cdot \underbrace{\frac{\gamma_{\infty}}{L g_{\infty} u_{\infty}}}_{1/Re}$$

11.10

In a gas flow the heat transfer is determined from the viscous effects and from heat conduction. The influencing quantities are the heat conductivity $\lambda \left[\frac{k \cdot g \cdot m}{s^3 \cdot K} \right]$, the dynamic viscosity $\eta \left[\frac{kg}{ms} \right]$ and the reference values for the temperature, the velocity, and the length. The physical relationship can be described with the energy equation

$$\boxed{\lambda \frac{\partial^2 T}{\partial y^2} + \eta \left(\frac{\partial u}{\partial y} \right)^2 = 0.}$$

$$\textcircled{1} \quad T_{ref} = T_R ; \quad L_{ref} = l ; \quad u_{ref} = u_R$$

$$\Rightarrow \bar{T} = \frac{T}{T_R} ; \quad \bar{y} = \frac{y}{l} ; \quad \bar{u} = \frac{u}{u_R}$$

$$\Rightarrow \boxed{\lambda \cdot \frac{T_R}{l^2} \cdot \frac{\partial^2 \bar{T}}{\partial \bar{y}^2} + \eta \cdot \frac{u_R^2}{l^2} \left(\frac{\partial \bar{u}}{\partial \bar{y}} \right)^2 = 0}$$

$$\textcircled{2} \quad \Rightarrow \boxed{\frac{\partial^2 \bar{T}}{\partial \bar{y}^2} + \frac{\eta \cdot u_R^2}{\lambda \cdot T_R} \left(\frac{\partial \bar{u}}{\partial \bar{y}} \right)^2 = 0}$$

$$\Downarrow \\ K = \frac{\eta \cdot u_R^2}{\lambda \cdot T_R}$$

$$\Gamma \text{ using } c_p = \frac{R}{\gamma - 1} :$$

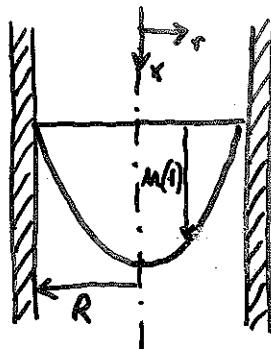
$$K = \frac{\eta \cdot c_p}{\lambda} \cdot \frac{u_R^2}{c_p \cdot T_R} = \underbrace{\frac{\eta \cdot c_p}{\lambda}}_{R_f} \underbrace{\frac{u_R^2}{\gamma R T_R}}_{Ma^2} (\gamma - 1)$$

$$R_f = Ma^2 \cdot (\gamma - 1)$$

example: laminar pipe flow

$$-\frac{\partial p}{\partial x} + \bar{g}g + \frac{2}{r} \frac{d}{dr} \left(r \frac{du}{dr} \right)$$

$$\bar{g} \downarrow$$



Determine the dimensionless parameters of the flow-problem.

$$\bar{p} = \frac{p}{\Delta p}; \bar{x} = \frac{x}{L}; \bar{s} = \frac{s}{s_{ref}}; \bar{g} = \frac{g}{g_{ref}}; \bar{\eta} = \frac{\eta}{\eta_{ref}}; \bar{r} = \frac{r}{R}; \bar{u} = \frac{u}{U_m}$$

$$\Rightarrow -\frac{\Delta p}{L} \frac{d\bar{p}}{d\bar{x}} + s_{ref} g_{ref} \cdot \bar{g} \bar{s} + \frac{\eta_{ref}}{R^2} U_m \cdot \frac{\bar{r}}{\bar{r}} \cdot \frac{d}{d\bar{r}} \left(\bar{r} \frac{d\bar{u}}{d\bar{r}} \right) = 0$$

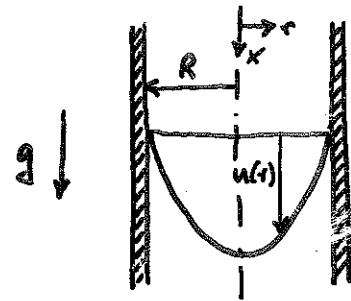
$$\Rightarrow -\underbrace{\frac{\Delta p \cdot R^2}{L \cdot \eta_{ref} \cdot U_m}}_{K_1} \frac{d\bar{p}}{d\bar{x}} + \underbrace{\frac{s_{ref} \cdot g_{ref} \cdot R^2}{\eta_{ref} \cdot U_m}}_{K_2} \cdot \bar{g} \bar{s} + \frac{2}{\bar{r}} \frac{d}{d\bar{r}} \left(\bar{r} \frac{d\bar{u}}{d\bar{r}} \right) = 0$$

$$K_1 = \frac{\Delta p}{s_{ref} \cdot U_m^2} \cdot \frac{s_{ref} \cdot U_m \cdot R}{\eta_{ref}} \cdot \frac{R}{L} = Eu \cdot Re \cdot \frac{R}{L}$$

$$K_2 = \frac{s_{ref} \cdot U_m \cdot R}{\eta_{ref}} \cdot \frac{g_{ref} \cdot R}{U_m^2} = Re \cdot \frac{1}{Fr^2}$$

example: laminar pipe flow

Determine the characterizing parameters of this problem.



Hint: μ_m, l, R

- ① physical quantities: $\Delta p, g, \mu_m, \eta, l, R, g \rightarrow k = 7$
- ② basic dimensions: $\left[\frac{\Delta p}{s^2 m}\right], \left[\frac{g}{m s}\right], \left[\frac{m}{s}\right], \left[\frac{\eta}{m s}\right], [m], [m], \left[\frac{m}{s^2}\right] \rightarrow r = 3$
- ③ number of parameters: $m = k - r = 4$
- ④ recurring variables: $g \left[\frac{m}{s^2}\right], \mu_m \left[\frac{m}{s}\right], R [m]$
- ⑤ $K_1 = \Delta p \cdot g^{\alpha_1} \cdot \mu_m^{\beta_1} \cdot R^{\gamma_1}$
- $K_2 = \eta \cdot g^{\alpha_2} \cdot \mu_m^{\beta_2} \cdot R^{\gamma_2}$
- $K_3 = l \cdot g^{\alpha_3} \cdot \mu_m^{\beta_3} \cdot R^{\gamma_3}$
- $K_4 = g \cdot g^{\alpha_4} \cdot \mu_m^{\beta_4} \cdot R^{\gamma_4}$
- ⑥
- | | | | |
|--|---|--|---|
| $K_1:$
$\begin{array}{c cc} \text{lg} & 1 + \alpha_1 \\ \hline m & -1 - 3\alpha_1 + \beta_1 + \gamma_1 \\ 5 & 2 & -\beta_1 \end{array}$ | $\begin{array}{c cc} \text{lg} & 1 + \alpha_2 \\ \hline m & -1 - 3\alpha_2 + \beta_2 + \gamma_2 \\ 5 & -1 & -\beta_2 \end{array}$ | $\begin{array}{c cc} \text{lg} & 1 + \alpha_3 \\ \hline m & -3\alpha_3 + \beta_3 + \gamma_3 \\ 5 & -\beta_3 \end{array}$ | $\begin{array}{c cc} \text{lg} & 1 + \alpha_4 \\ \hline m & -3\alpha_4 + \beta_4 + \gamma_4 \\ 5 & -2 & -\beta_4 \end{array}$ |
|--|---|--|---|
- $\left. \begin{array}{l} \alpha_1 = -1, \beta_1 = -2, \gamma_1 = 0 \\ K_1 = \frac{\Delta p}{\mu_m^2} = Eu \end{array} \right\}$
 $\left. \begin{array}{l} \alpha_2 = -1, \beta_2 = -1, \gamma_2 = -1 \\ K_2 = \frac{\eta}{\mu_m R} = \frac{1}{Re} \end{array} \right\}$
 $\left. \begin{array}{l} \alpha_3 = 0, \beta_3 = 0, \gamma_3 = 1 \\ K_3 = \frac{l}{R} \end{array} \right\}$
 $\left. \begin{array}{l} \alpha_4 = 0, \beta_4 = -2, \gamma_4 = 1 \\ K_4 = \frac{g \cdot D}{\mu_m^2} = \frac{1}{Fr^2} \end{array} \right\}$